IN THE CLAIMS

The claims have been amended as follows:

1. A process to isomerize hydrocarbon feedstreams comprising:

a) contacting a hydrocarbon feedstream with a ~~aqueous-treated~~ catalyst comprising ferrierite, or a zeolite isostructural to ferrierite, under hydroisomerization conditions including:

i) temperatures of about 400 to about 800°F(205°C to about 430°C); and

ii) pressures of about 400 to about 2000 psig(2860 to about 13890 kPa);

~~wherein after the above-described method, said catalyst desorbs sorbed ammonia at a temperature about 248°F(120°C) lower than the same untreated catalyst before the above-described method.~~ **wherein said catalyst is an aqueous treated catalyst resulting from subjecting said catalyst to an aqueous treatment conducted under conditions such that the aqueous-treated catalyst shows removal of sorbed ammonia at a temperature about 248°F(120°C) lower than the same untreated catalyst and wherein said aqueous treatment comprises i) submersing said catalyst in water for less than about 24 hours at a temperature of about 210°F to about 575°F (100 to about 300°C); and ii) adjusting the pH of the water to about 2 to about 7 through the addition of an acidic or basic material that does not have a deleterious effect on said aqueous-treated catalyst.**

2. The process according to claim 1 wherein said hydrocarbon feedstream is a C_{10+} hydrocarbon feedstream boiling in the range of about 345°F to about 1050°F.

3. The process according to claim 1 wherein said hydrocarbon feedstream is a C_{9-} hydrocarbon feedstream boiling below about 345°F.

4. The process according to ~~any of the~~ claim 1 wherein said aqueous-treated catalyst further comprises about 0.05 to about 2.0 wt.%, based on the catalyst, of at least one Group VIII metal.

5. The process according to ~~Claim~~ claim 4 wherein said Group VIII metal is a Group VIII noble metal.

6. The process according to ~~Claim~~ claim 5 wherein said Group VIII metal is Pt.

7. **Canceled.**

8. **Canceled.**

~~9.~~7. The process according to ~~Claim 8~~ claim 6 wherein said basic material is dilute aqueous ammonium hydroxide, and said acidic material is dilute hydrochloric acid.

~~10.~~8. The process according to claim ~~8~~ 7 wherein the product selectivity of the hydroisomerization process improves by more than about 20%.

~~11.~~ 9. The process according to claim ~~9~~ 7 wherein the product selectivity of the hydroisomerization process improves by more than about 30%.

~~12.~~ 10. The process according to claim ~~10~~ 8 wherein the product selectivity of the hydroisomerization process improves by more than about 50%.

~~13.~~ 11. The process according to ~~any of the Claim~~ claim 6 wherein said aqueous-treated catalyst is treated after the addition of the metals.

~~14.~~ 12. The process according to ~~Claim 13~~ claim 11 wherein said aqueous-treated catalyst further comprises at least one binder or matrix material selected from clays, silica, and alumina.

~~15.~~ 13. The process according to ~~Claim 14~~ claim 12 wherein said binder or matrix material is alumina present in a ratio of less than about 15 parts zeolite to one part binder.

~~16.~~ 14. The process according to ~~Claim 9~~ claim 7 wherein said water treatment does not result in the dealumination of said ferrierite.

~~17.~~ 15. A process to isomerize hydrocarbon feedstreams comprising:

a) contacting a hydrocarbon feedstream with a ~~aqueous-treated~~ catalyst comprising ferrierite, or a zeolite isostructural to ferrierite, and about 0.05 to about 2.0wt.% of at least one Group VIII metal, based on the weight of the catalyst, under hydroisomerization conditions including:

i) temperatures of about 400 to about 800°F(205°C to about 430°C); and

ii) pressures of about 400 to about 2000 psig(2860 to about 13890 kPa);

wherein said ~~aqueous-treated~~ catalyst is an aqueous treated catalyst resulting from subjecting said catalyst to an aqueous treatment conducted under conditions such that the aqueous-treated catalysts show removal of sorbed ammonia at a temperature about 194°F to about 230°F(90 to about 110°C) lower than the same untreated catalyst, and wherein said aqueous treatment comprises i) submersing said catalyst in water for less than about 24 hours at a temperature of about 210°F to about 575°F (100 to about 300°C); and ii) adjusting the pH of the water to about 2 to about 7 through the addition of an acidic or basic material that does not have a deleterious effect on said aqueous-treated catalyst.

~~18.~~ 16. The process according to claim ~~17~~ 15 wherein said hydrocarbon feedstream is a C_{10+} hydrocarbon feedstream boiling in the range of about 345°F to about 1050°F.

~~19.~~ 17. The process according to claim ~~17~~ 15 wherein said hydrocarbon feedstream is a C_9- hydrocarbon feedstream boiling below about 345°F.

~~20.~~ 18. The process according to ~~Claim 17~~ claim 15 wherein said Group VIII metal is a Group VIII noble metal.

~~21.~~ 19. The process according to ~~Claim 20~~ claim 18 wherein said Group VIII metal is Pt.

~~22.~~ 20. The process according to ~~Claim 21~~ claim 19 wherein said aqueous-treated catalyst is subjected to an aqueous treatment comprising submersing said aqueous-treated in catalyst in water for less than about 20 hours at a temperature of 284°F to about 500°F(140 to about 260°C).

23. **Canceled.**

24. **Canceled.**

~~25.~~ 21. The process according to ~~Claim 21~~ claim 19 wherein said aqueous-treated catalyst further comprises at least one binder or matrix material selected from clays, silica, and alumina.

~~26.~~ 22. The process according to ~~Claim 24~~ claim 21 wherein said aqueous treatment does not result in the dealumination of said ferrierite.

~~27.~~ 23. The process according to ~~Claim 26~~ claim 22 wherein the product selectivity of the hydroisomerization process improves by more than about 20%.

1. A process to isomerize hydrocarbon feedstreams comprising:

a) contacting a hydrocarbon feedstream with a catalyst comprising ferrierite, or a zeolite isostructural to ferrierite, under hydroisomerization conditions including:

i) temperatures of about 400 to about 800°F(205°C to about 430°C); and

ii) pressures of about 400 to about 2000 psig(2860 to about 13890 kPa);

wherein said catalyst is an aqueous treated catalyst resulting from subjecting said catalyst to an aqueous treatment conducted under conditions such that the aqueous-treated catalyst shows removal of sorbed ammonia at a temperature about 248°F(120°C) lower than the same untreated catalyst and wherein said aqueous treatment comprises i) submersing said catalyst in water for less than about 24 hours at a temperature of about 210°F to about 575°F (100 to about 300°C); and ii) adjusting the pH of the water to about 2 to about 7 through the addition of an acidic or basic material that does not have a deleterious effect on said aqueous-treated catalyst.

2. The process according to claim 1 wherein said hydrocarbon feedstream is a C_{10+} hydrocarbon feedstream boiling in the range of about 345°F to about 1050°F.

3. The process according to claim 1 wherein said hydrocarbon feedstream is a C_{9-} hydrocarbon feedstream boiling below about 345°F.

4. The process according to claim 1 wherein said aqueous-treated catalyst further comprises about 0.05 to about 2.0 wt.%, based on the catalyst, of at least one Group VIII metal.

5. The process according to claim 4 wherein said Group VIII metal is a Group VIII noble metal.

6. The process according to claim 5 wherein said Group VIII metal is Pt.

7. The process according to claim 6 wherein said basic material is dilute aqueous ammonium hydroxide, and said acidic material is dilute hydrochloric acid.

8. The process according to claim 7 wherein the product selectivity of the hydroisomerization process improves by more than about 20%.

9. The process according to claim 7 wherein the product selectivity of the hydroisomerization process improves by more than about 30%.

10. The process according to claim 8 wherein the product selectivity of the hydroisomerization process improves by more than about 50%.

11. The process according to claim 6 wherein said aqueous-treated catalyst is treated after the addition of the metals.

12. The process according to claim 11 wherein said aqueous-treated catalyst further comprises at least one binder or matrix material selected from clays, silica, and alumina.

13. The process according to claim 12 wherein said binder or matrix material is alumina present in a ratio of less than about 15 parts zeolite to one part binder.

14. The process according to claim 7 wherein said water treatment does not result in the dealumination of said ferrierite.

15. A process to isomerize hydrocarbon feedstreams comprising:

a) contacting a hydrocarbon feedstream with a catalyst comprising ferrierite, or a zeolite isostructural to ferrierite, and about 0.05 to about 2.0wt.% of at least one Group VIII metal, based on the weight of the catalyst, under hydroisomerization conditions including:

i) temperatures of about 400 to about 800°F(205°C to about 430°C); and

ii) pressures of about 400 to about 2000 psig(2860 to about 13890 kPa);

wherein said catalyst is an aqueous treated catalyst resulting from subjecting said catalyst to an aqueous treatment conducted under conditions such that the aqueous-treated catalysts show removal of sorbed ammonia at a temperature about 194°F to about 230°F(90 to about 110°C) lower than the same untreated catalyst, and wherein said aqueous treatment comprises i) submersing said catalyst in water for less than about 24 hours at a temperature of about 210°F to about 575°F (100 to about 300°C); and ii) adjusting the pH of the water to about 2 to about 7 through the addition of an acidic or basic material that does not have a deleterious effect on said aqueous-treated catalyst.

16. The process according to claim 15 wherein said hydrocarbon feedstream is a C_{10+} hydrocarbon feedstream boiling in the range of about 345°F to about 1050°F.

17. The process according to claim 15 wherein said hydrocarbon feedstream is a C_{9-} hydrocarbon feedstream boiling below about 345°F.

18. The process according to claim 15 wherein said Group VIII metal is a Group VIII noble metal.

19. The process according to claim 18 wherein said Group VIII metal is Pt.

20. The process according to claim 19 wherein said aqueous-treated catalyst is subjected to an aqueous treatment comprising submersing said aqueous-treated in catalyst in water for less than about 20 hours at a temperature of 284°F to about 500°F(140 to about 260°C).

21. The process according to claim 19 wherein said aqueous-treated catalyst further comprises at least one binder or matrix material selected from clays, silica, and alumina.

22. The process according to claim 21 wherein said aqueous treatment does not result in the dealumination of said ferrierite.

23. The process according to claim 22 wherein the product selectivity of the hydroisomerization process improves by more than about 20%.